



# Pd-SnO<sub>2</sub> interface enables synthesis of syngas with controllable H<sub>2</sub>/CO ratios by electrocatalytic reduction of CO<sub>2</sub>

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## ABSTRACT

Electrochemical CO<sub>2</sub> reduction reaction (eCO<sub>2</sub>RR) to syngas (CO + H<sub>2</sub>) is considered as a great potential and efficient way to abate carbon emissions and mitigate the depletion of fossil resources. Herein, a series of Pd-loaded SnO<sub>2</sub> nanosheets catalysts (Pd-SnO<sub>2</sub> NSs) are developed by photodeposition of Pd on the surface of SnO<sub>2</sub> nanosheets. Due to the formation of the active Pd-SnO<sub>2</sub> interface, the as-prepared Pd-SnO<sub>2</sub> catalysts exhibit a suppressed eCO<sub>2</sub>RR to HCOOH pathway, thus realizing the faradaic efficiency of syngas close to 100%. The obtained optimal 4.3Pd-SnO<sub>2</sub> catalyst exhibits high CO selectivity (78% FE<sub>CO</sub>) and wide H<sub>2</sub>/CO ratio ranged from 4.2 to 0.28. Notably, the H<sub>2</sub>/CO ratio can be controlled easily by adjusting the applied potential. Moreover, the H<sub>2</sub>/CO ratio can maintain for more than 30 h. This work unfolds a promising candidate for earth-abundant Sn-based electrocatalysts for eCO<sub>2</sub>RR to syngas.

## 1. Introduction

As an important raw material, syngas (CO + H<sub>2</sub>) can produce various value-added chemical feedstocks and hydrocarbons through the industrial processes (e.g. Fischer-Tropsch synthesis) [1–5]. Traditionally, the industrial generation of syngas is primarily relied on the water-gas shift reaction of non-renewable fossil fuels (such as coal, oil, and natural gas), which requires huge energy investment and harsh conditions [6–9]. Therefore, to develop sustainable syngas production technique is highly required to substitute the facing-exhausted fossil fuels. The electrochemical CO<sub>2</sub> reduction reaction (eCO<sub>2</sub>RR) is considered as the clean and promising method to produce CO [10–16]. Besides, the hydrogen evolution reaction (HER), which takes place in the same range of potentials as eCO<sub>2</sub>RR as a competitive reaction, is also a green method to generate H<sub>2</sub> [17–22]. Taking the advantage of mild and controllable reaction condition during eCO<sub>2</sub>RR process, syngas generation can greatly help reduce energy consumption and pollution. Moreover, if a CO:H<sub>2</sub> ratio can be controlled to the desired ratio for the existing thermo-catalytic process, for example, when the ratios of H<sub>2</sub>/CO are 0.6 and 2, the syngas has been widely used for Fischer-Tropsch reaction and

methanol synthesis [23–26]. Thus, growing efforts have been devoted to develop electrocatalysts for the transformation of CO<sub>2</sub> and H<sub>2</sub>O towards syngas with controllable ratios and high activity.

To date, many metals and their oxide-derived nanomaterials (e.g., Ag, Au, Sn, Bi, etc.), have been investigated as electrocatalysts for eCO<sub>2</sub>RR in search of a viable process for recycling CO<sub>2</sub> [27–30]. Among them, tin dioxide (SnO<sub>2</sub>) represents one of the most promising catalysts, owing to its high-activity for eCO<sub>2</sub>RR, low cost and environmentally friendly [31,32]. However, the efficiency of CO generation is greatly hampered by series of by-products, including formic acid, methane, methanol, etc [33–36]. Especially, the formation of high percentage of formic acid in the eCO<sub>2</sub>RR on a tin-based catalyst consumes a lot of electricity, consequently, reduces the energy efficiency, which hinders efficient production of target syngas. Thus, a great deal of attention has been paid to the development of eCO<sub>2</sub>RR catalysts that have high selectivity for CO and HER activity. It is widely accepted that the selectivity is highly dependent on the surface and interface electronic structure of catalysts, especially the local charge density redistribution of metals at active sites, which can be tailored through the doping of heteroatoms or interacting with foreign metal atoms [37–39]. For

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example, Chen and co-workers constructed Sn–Ti–O interfaces for the electron-density transfer from Ti to Sn, which enhances the dissociative adsorption of  $^*\text{COOH}$  intermediate and results in producing CO instead of HCOOH [13]. Zheng and co-workers demonstrated a 2D hierarchical Pd/SnO<sub>2</sub> structure met a demand on balancing CO adsorption and activation for electroreduction of CO<sub>2</sub> to CH<sub>3</sub>OH via a multi-electron transfer process [36]. Though Pd shows high activity for eCO<sub>2</sub>RR and HER, the strong CO adsorption limits its practical application [40,41]. Therefore, establishing a counterpoise Pd-SnO<sub>2</sub> interface to tailor the electronic structures of the active metal sites has great potential to control the eCO<sub>2</sub>RR and HRE processes, suppressing the HCOOH selectivity, thus achieving the production of syngas with controllable H<sub>2</sub>/CO ratios.

Herein, we develop a facile preparation of Pd-modified SnO<sub>2</sub> nanosheets catalysts (Pd-SnO<sub>2</sub> NSs) for efficient syngas production with widely tunable H<sub>2</sub>/CO ratios. Large-size SnO<sub>2</sub> NSs provide a high specific area for supporting Pd nanoparticles, thereby exposing more active interface. With the increasing of Pd-SnO<sub>2</sub> interface, the eCO<sub>2</sub>RR to HCOOH pathway is greatly suppressed. Pd-SnO<sub>2</sub> NSs display high activity, as well as desirable current density and stability for CO<sub>2</sub> reduction to CO. Most importantly, the ratios of CO to H<sub>2</sub> in the products can be easily manipulated by varying the applied potential. The H<sub>2</sub>/CO ratios range from 4.2 to 0.28 in 4.3Pd-SnO<sub>2</sub> catalyst, when the applied potentials vary from  $-0.5$  to  $-1.1$  V. The H<sub>2</sub>/CO ratio can effectively maintain under a long-term durability test of 30 h. Electrochemical test and theory calculations demonstrate that the formation of Pd-SnO<sub>2</sub> interface can lead the charge density redistribution of catalytic interfaces and change the energy-favorable intermediates adsorption from  $^*\text{OCHO}$  in SnO<sub>2</sub> NSs to  $^*\text{COOH}$  on Pd-SnO<sub>2</sub> NSs, thus improving the selectivity of CO with wide range of H<sub>2</sub>/CO ratios for syngas production.

## 2. Experimental section

### 2.1. Chemicals and materials

Tin(IV) chloride pentahydrate (SnCl<sub>4</sub>·5H<sub>2</sub>O), palladium(II) nitrate, ethylene glycol, ethanol, N-ethyl-4-piperidinecarboxamide hydrochloride, and potassium bicarbonate (KHCO<sub>3</sub>) were bought from Sinopharm (Shanghai, China). Nafion solution, Nafion®117 film and nafion solution were obtained from Alfa Aesar.

### 2.2. Preparation of SnO<sub>2</sub> NSs

The procedure of the preparation of SnO<sub>2</sub> NSs is illustrated in Scheme 1. Firstly, graphene oxide (GO) nanosheets were fabricated by a typical method [42]. Then, the as-prepared GO nanosheets (15 mg) and SnCl<sub>4</sub> (0.75 mmol) were mixed in a 150 mL pH 2.2 buffer solution (2.07 g glycinesodium hydroxide and 462 mL ethylene glycol in an 88 mL H<sub>2</sub>O and 2 mL HCl) and dispersed by ultrasound for 15 min. Subsequently, the mixture was vigorously stirred at 70 °C for 4 h to get the SnO<sub>2</sub>-GO precursor. Finally, The SnO<sub>2</sub> NSs were obtained by calcining the

SnO<sub>2</sub>-GO precursor and removing the GO templates.

### 2.3. Preparation of Pd-SnO<sub>2</sub> NSs

The different content of Pd-SnO<sub>2</sub> NSs were preparation by photo-deposition method. Specifically, SnO<sub>2</sub> NSs (20 mg) were added in the mixed solution of ethyl alcohol (10 mL) and H<sub>2</sub>O (100 mL) and treated with ultrasound for 15 min at room temperature. Then, Pd<sup>2+</sup> aqueous solution with different concentrations was slowly added drop by drop under vigorously stirring for 30 min at dark conditions. Subsequently, the solution was transferred to a photocatalytic reaction chamber equipped with a 350 W xenon lamp and irradiated the suspension for 4 h under continuous agitation. The color of the suspension changed from yellow to dark gray, indicating that the Pd had been loaded on the surface of SnO<sub>2</sub> NSs. The gray powder after centrifugation of suspension was washed three times with deionized water and ethanol, respectively. Finally, the powder was dried overnight at 80 °C to get Pd-SnO<sub>2</sub> NSs.

### 2.4. Electrochemical measurements

The electrochemical measurements were performed in the CO<sub>2</sub>-saturated 0.5 M KHCO<sub>3</sub> electrolyte with Nafion-membrane separated airtight H-type cell, where Ag/AgCl electrode and Pt electrode were used as the reference electrode and counter electrode, respectively. The working electrode was prepared by immobilization of the electrocatalyst on carbon paper (1.5 cm × 0.5 cm). Typically, electrocatalyst (10 mg) and Nafion solution (50 μL 5 wt%) were dispersed in the mixed solution of 0.5 mL ethanol and 0.5 mL H<sub>2</sub>O with sonicating for 20 min to form a homogeneous catalyst ink. Then, the catalyst ink (50 μL) was uniformly deposited on a piece of carbon paper (1.0 cm × 0.5 cm) to act as the working electrode. The potentials reported are all converted into reversible hydrogen electrode (RHE).  $E(\text{RHE}) = E(\text{Ag}/\text{AgCl}) + 0.1989 \text{ V} + 0.059 \times \text{pH}$ .

### 2.5. DFT models and calculations

The free energies of CO<sub>2</sub> reduction states were calculated by using codes from Vienna Ab-initio Simulation Package (VASP). The projector augmented wave (PAW) pseudopotential with the PBE generalized gradient approximation (GGA) exchange correlation function. For all the geometry optimizations, the cutoff energy of the plane waves basis set was 500 eV and a Monkhorst-Pack mesh of  $3 \times 3 \times 1$  was used in K-sampling in the adsorption energy calculation and  $7 \times 7 \times 1$  was used in K-sampling in the density of state (DOS) calculation. All atoms were fully relaxed with the energy convergence tolerance of  $10^{-5}$  eV per atom, and the final force on each atom was  $< 0.05$  eV Å<sup>-1</sup>. All periodic slabs have a vacuum layer of at least 15 Å. The bottom layer of atoms was fixed at their optimized bulk-truncated positions during geometry optimization, and the rest of atoms could relax. The adsorption energy of reaction intermediates can be calculated using the following equation:

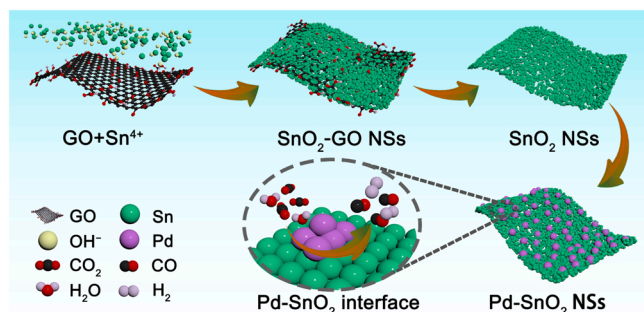
$$\Delta E = E_{\text{ads}} - E^*, \Delta G = \Delta E + \Delta E_{\text{ZPE}} - T\Delta S,$$

Where,  $\Delta E_{\text{ZPE}}$  is the zero-point energy change,  $\Delta S$  is the entropy change. In this work, the values of  $\Delta E_{\text{ZPE}}$  and  $\Delta S$  were obtained by vibration frequency calculation.

## 3. Results and discussion

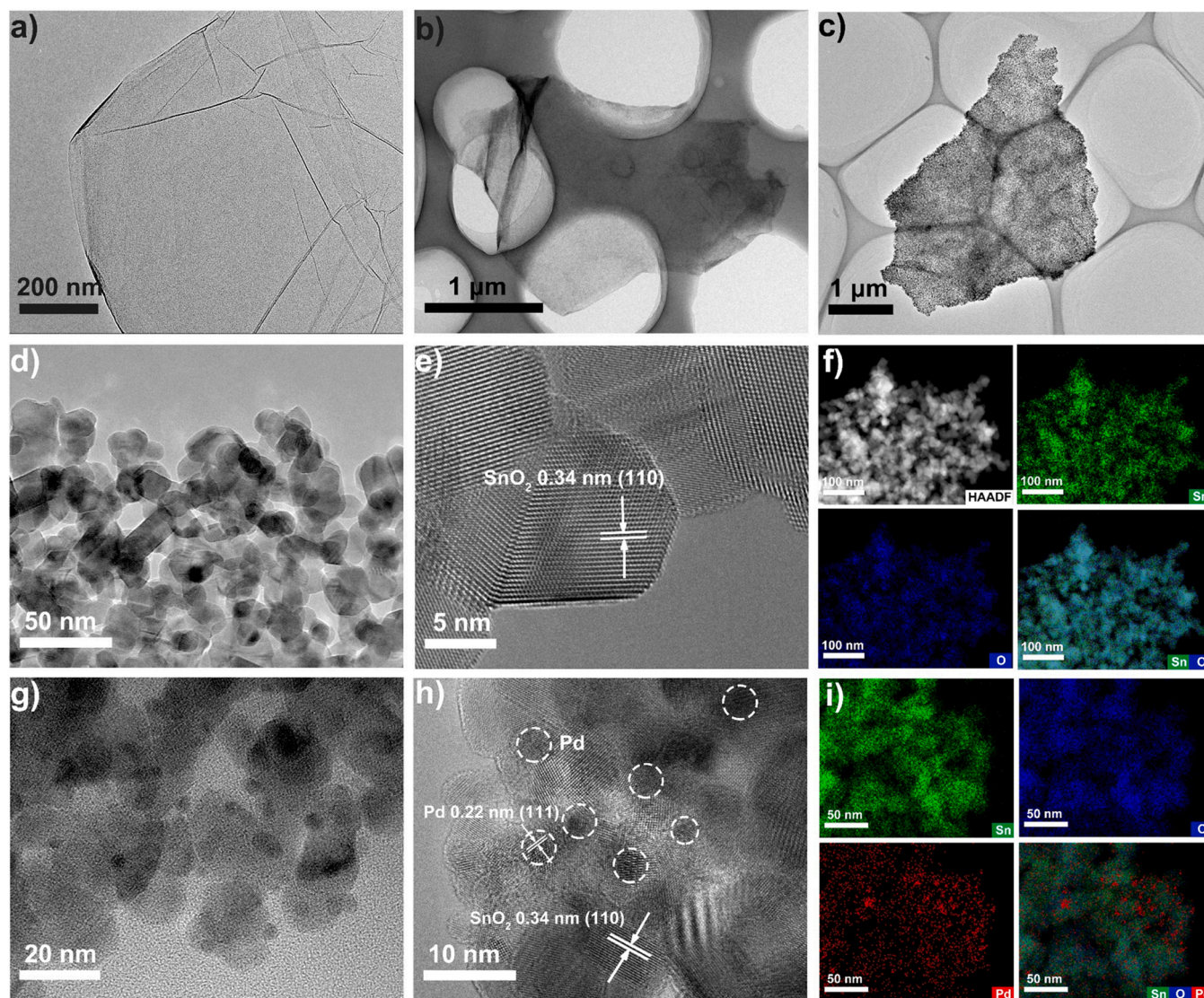
### 3.1. Synthesis and characterizations of the catalysts

To characterize the structures of the as-prepared samples, the transmission electron microscopy (TEM) characterizations were carried out. As shown in Fig. 1a & b, SnO<sub>2</sub>-GO NSs precursors possess large-size ultrathin morphology, like that of the GO NSs template. The sizes of SnO<sub>2</sub>-GO NSs are about 3–5 μm. After calcining the SnO<sub>2</sub>-GO precursor,



Scheme 1. Schematic illustration of the synthesis process of Pd-SnO<sub>2</sub> NSs.





**Fig. 1.** Synthesis and structural characterization. TEM image of a) GO NSs, b) SnO<sub>2</sub>-GO NSs, c) SnO<sub>2</sub> NSs. d) high-magnification TEM image, e) high-resolution TEM image and f) corresponding elemental mappings of SnO<sub>2</sub> NSs. g) TEM image, h) high-resolution TEM image and i) corresponding elemental mappings of Pd-SnO<sub>2</sub> NSs.

the GO NSs were removed, and the as-obtained SnO<sub>2</sub> NSs remain large-size two-dimensional structures (Fig. 1c & d). The high-resolution TEM (HR-TEM) image in Fig. 1e displays a clear interplanar spacing of 0.34 nm, ascribing to the (1 1 0) facet of the tetragonal SnO<sub>2</sub>. Meanwhile, the high-angle annular darkfield scanning transmission electron microscopy (HAADF-STEM) analysis for SnO<sub>2</sub> NSs exhibit that Sn and O elements are distributed uniformly on the nanosheets (Fig. 1f). As shown in Fig. 1d, SnO<sub>2</sub> NSs are mainly composed of small SnO<sub>2</sub> particles, which leads to a rough surface, in favour of increasing the surface area. Thus, Pd can be anchored on the surface of SnO<sub>2</sub> NSs via photo-deposition method. As shown in Fig. S1 and Fig. 1g, Pd-SnO<sub>2</sub> NSs possess also 2D large sizes morphology. The Pd nanoparticles with an average diameter of about 4 nm are uniformly attached on the surface of SnO<sub>2</sub> NSs. In comparison with SnO<sub>2</sub> NSs, Pd-SnO<sub>2</sub> NSs exhibits lattice fringes with a d-spacing of 0.34 and 0.22 nm (Fig. 1h), corresponding to the (110) facet of SnO<sub>2</sub> and the (111) plane of Pd, respectively. The successful loading of Pd into SnO<sub>2</sub> supports are also confirmed by the elemental mappings. Besides Sn and O elements, the uniform Pd element is observed in the corresponding elemental mappings of Pd-SnO<sub>2</sub> NSs (Fig. 1i).

To further elucidate the structural and chemical information of the Pd-SnO<sub>2</sub> NSs catalysts, inductively coupled plasma optical emission spectrometry (ICP-OES), X-ray diffraction (XRD) and Raman

spectroscopy were preformed. The Pd-SnO<sub>2</sub> catalysts are denoted as xPd-SnO<sub>2</sub> (x: weight percentage of Pd in the catalyst). According to the ICP-OES analysis, the Pd contents in 2.2Pd-SnO<sub>2</sub>, 4.3Pd-SnO<sub>2</sub> and 7.5Pd-SnO<sub>2</sub> catalysts are 2.2%, 4.3% and 7.5%, respectively. The crystalline structures of SnO<sub>2</sub> NSs and Pd-SnO<sub>2</sub> NSs are presented in Fig. 2a. SnO<sub>2</sub> NSs supports only exhibit the peaks of the SnO<sub>2</sub> crystalline lattice (JCPDS No. 41-1445). Meanwhile, no characteristic diffraction peaks of Pd or PdO were found in the XRD patterns of 2.2Pd-SnO<sub>2</sub> and 4.3Pd-SnO<sub>2</sub> catalyst, which can be attributed to the trace Pd loading beyond the detection limit of XRD [43,44]. When the Pd content increases to 7.5%, a weak characteristic peak of Pd is observed at 7.5% Pd-SnO<sub>2</sub> NSs, which is consistent with the Pd crystalline lattice (JCPDS No. 46-1043). Furthermore, the Raman spectroscopy of SnO<sub>2</sub> NSs exhibits three characteristic fingerprint peaks at 507.5, 633.2 and 773.7 cm<sup>-1</sup>, corresponding to the three Raman active phonon modes: E<sub>g</sub>, A<sub>1g</sub> and B<sub>2g</sub> of SnO<sub>2</sub> [45]. After the deposition of Pd on the SnO<sub>2</sub> surface, all Raman active phonon modes of SnO<sub>2</sub> obviously shift to the lower wavelength. This is attributed to the surface plasmon resonance from Pd-modification on SnO<sub>2</sub> surface, indicating that specific electromagnetic interact exists in the Pd metal and SnO<sub>2</sub> semiconductor surface.

The composition analysis was conducted by X-ray photoelectron spectroscopy (XPS), which were calibrated via its C1s reference value of

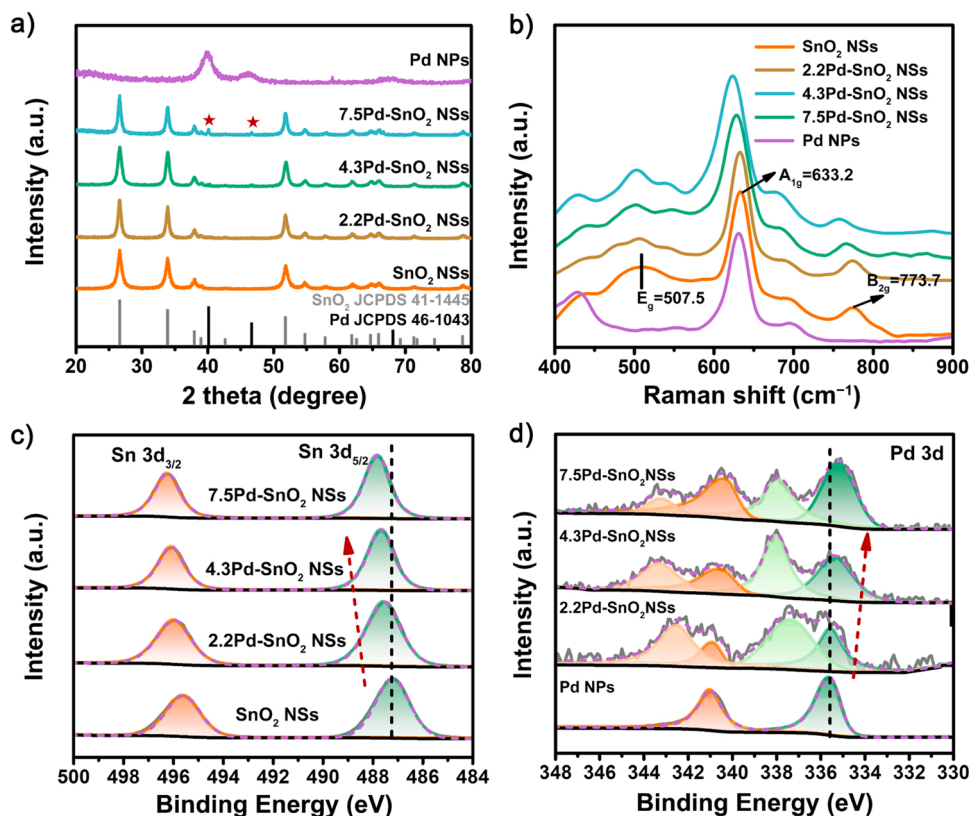


Fig. 2. a) XRD spectra and b) Raman spectroscopy of SnO<sub>2</sub> NSs, Pd-SnO<sub>2</sub> NSs and Pd NPs. c) Sn 3d XPS spectra of SnO<sub>2</sub> NSs, and Pd-SnO<sub>2</sub> NSs. d) Pd 3d XPS spectra of Pd NPs and Pd-SnO<sub>2</sub> NSs.

284 eV. The coexistence of Sn, O and Pd elements are clearly observed in the full-range XPS spectra for all Pd-SnO<sub>2</sub> NSs samples, comparing with that of the Pd free SnO<sub>2</sub> NSs sample (Fig. S2). Moreover, the high-resolution spectra of Sn 3d in Fig. S3 show that the two main peaks (495.61 and 487.18 eV in SnO<sub>2</sub> NSs, 495.95 and 487.54 eV in 2.2Pd-SnO<sub>2</sub> NSs, 496.06 and 487.68 eV in 4.3Pd-SnO<sub>2</sub> NSs, 496.29 and 487.79 eV in 7.5Pd-SnO<sub>2</sub> NSs), which can be assigned to the characteristic spin-orbit split Sn 3d<sub>3/2</sub> and 3d<sub>5/2</sub> oxidation state of SnO<sub>2</sub> [31]. Remarkably, the two peaks of Sn 3d shift to high binding energy with the increase of Pd content, indicating strong interaction and electron transfer in Pd-SnO<sub>2</sub> interface, due to the higher electronegativity of Pd than Sn. In the Pd 3d spectra of Pd NPs (Fig. S4), the 3d<sub>5/2</sub> and 3d<sub>3/2</sub> peak located at 335.09 and 340.45 eV are the characteristic of metallic Pd<sup>0</sup>. After the formation of Pd-SnO<sub>2</sub> interface, the two 3d peaks of Pd<sup>0</sup> shift to lower binding energy, implying an electron-rich state (Fig. 2d). Meanwhile, the Pd 3d spectra of Pd-SnO<sub>2</sub> NSs can fit with two components, in which the other two peaks are assigned to Pd(II) in the Pd-O state. The high-resolution O 1s XPS spectra of SnO<sub>2</sub> NSs exhibits two peaks at 532.08 and 531.09 eV, representing the O 1s peaks for O-H and O-Sn (Fig. S5). And a weak additional O-Pd peak at 533.36 eV are observed at Pd-SnO<sub>2</sub> NSs, confirming the successful immobilization of Pd on SnO<sub>2</sub> surface and the formation of Pd-O-Sn interaction. The above results demonstrate that the formation of Pd-SnO<sub>2</sub> interface promotes the strong electron transfer between Sn and Pd, and generates electron-rich state sites, which is helpful to coupling the electron-deficient \*COOH intermediates, thus enhancing the CO selectivity [46].

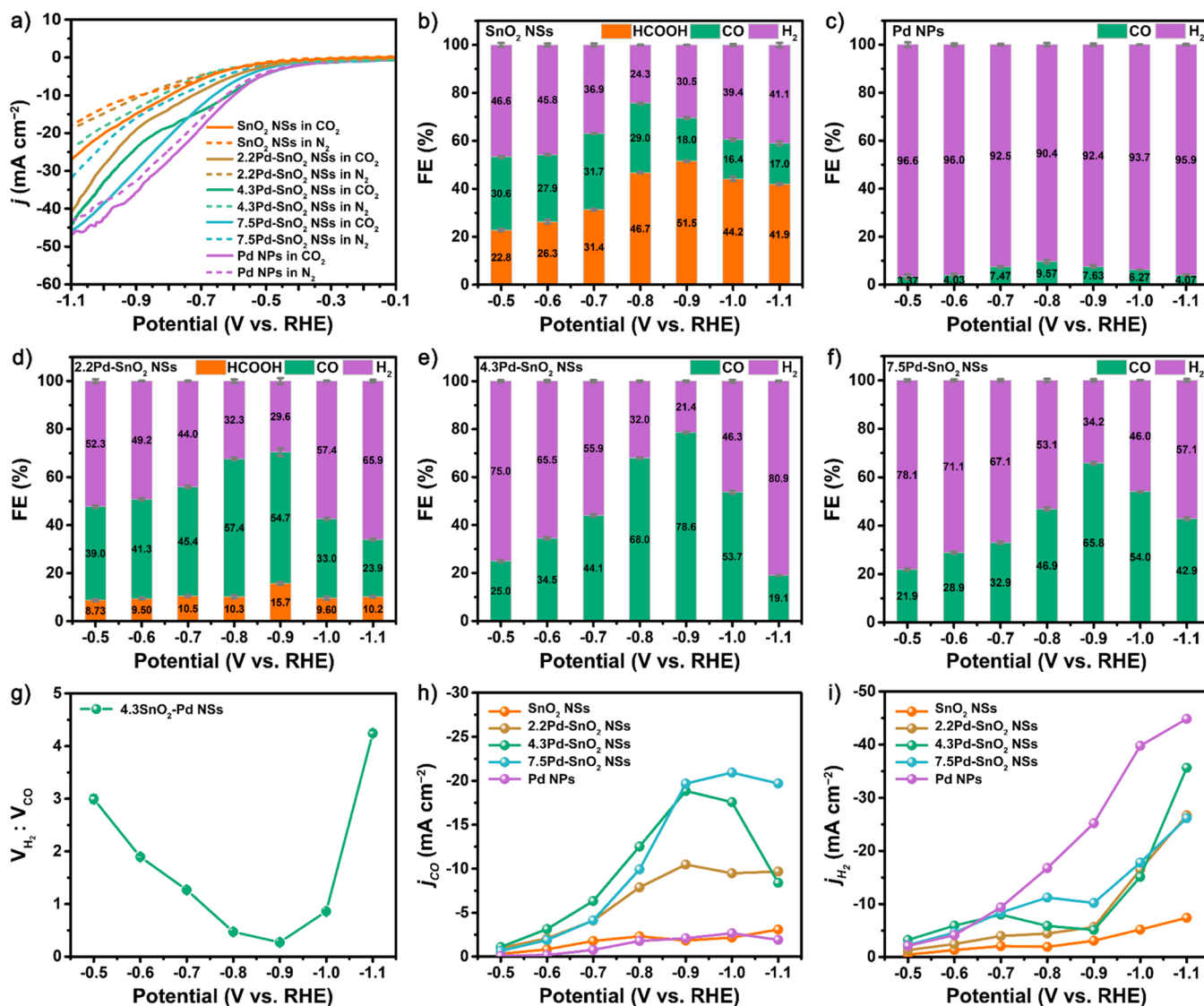
### 3.2. Electrocatalytic CO<sub>2</sub> reduction performance of the catalysts

The electrocatalytic performance of Pd-SnO<sub>2</sub> NSs for production of syngas was evaluated using Pd-SnO<sub>2</sub> NSs catalyst-modified carbon paper as a working electrode in a CO<sub>2</sub>-saturated 0.5 M KHCO<sub>3</sub> aqueous

solution. Linear sweep voltammetry (LSV) measurements are performed at scan rate of 50 mV s<sup>-1</sup>. It shows that SnO<sub>2</sub> NSs, Pd-SnO<sub>2</sub> NSs and Pd NPs catalysts exhibit higher current density in CO<sub>2</sub>-saturated than that in a N<sub>2</sub>-saturated aqueous solution, suggesting effective eCO<sub>2</sub>RR catalytic activity (Fig. S6). Significantly, the current densities in both CO<sub>2</sub>-saturated and N<sub>2</sub>-saturated solution increase gradually with the increase of the Pd content, suggesting that the Pd-SnO<sub>2</sub> interface can boost eCO<sub>2</sub>RR and HER and be favour of producing syngas (Fig. 3a). Moreover, the increase of the Pd content effectively reduce the overpotential of Pd-SnO<sub>2</sub> NSs, ascribing to the improved conductivity of the catalyst with the addition of Pd.

As shown in Fig. 3b, CO, HCOOH and H<sub>2</sub> are found in the products on SnO<sub>2</sub> NSs catalyst, where the Faraday efficiency (FE) of HCOOH reaches 22.8% – 51.5%. Such high production of HCOOH needs to consume a large amount of electricity, resulting in low energy efficiency and diminished selectivity for the target syngas. In contrast, only CO and H<sub>2</sub>, but no HCOOH produced upon Pd NPs. However, the proportion of CO is less than 10% at the applied potential, which is not suitable for the practical application (Fig. 3c). It is worthwhile to note that the FE of HCOOH gradually decreases with the increasing of the Pd content of Pd-SnO<sub>2</sub> (i.e., increasing the interface area of the catalyst). For example, upon 2.2Pd-SnO<sub>2</sub> NSs catalyst, the FE of HCOOH drops below 15.7% (Fig. 3d); while the total FE for CO + H<sub>2</sub> on 4.3Pd-SnO<sub>2</sub> catalyst and 7.5Pd-SnO<sub>2</sub> NSs reaches close to 100% (Fig. 3e & f). When the potential sweeps from -0.5 to -1.1 V, the FE<sub>CO</sub> on 4.3Pd-SnO<sub>2</sub> catalyst gradually increased to a maximum of 78.6% at -0.9 V (H<sub>2</sub>/CO ratio: 0.28); afterwards, the FE<sub>CO</sub> decreased, similar trend was observed on 7.5Pd-SnO<sub>2</sub> NSs. Distinctly, the maximum of FE<sub>CO</sub> on 7.5Pd-SnO<sub>2</sub> NSs is only 65.8% (H<sub>2</sub>/CO ratio: 0.52), which attributes to the fact that high Pd incorporation leads to a booming HER. As shown in Fig. 3g and Fig. S7, by adjusting applied potential (-0.5 to -1.1 V), the optimal 4.3Pd-SnO<sub>2</sub> catalyst exhibit a controllable H<sub>2</sub>/CO ratio ranged from 4.2 to 0.28, which is wider than that of SnO<sub>2</sub> NSs (2.4–0.83), 2.2Pd-SnO<sub>2</sub> NSs





**Fig. 3.** a) LSV curves of SnO<sub>2</sub> NSs, Pd-SnO<sub>2</sub> NSs and Pd NPs. FE on b) SnO<sub>2</sub> NSs, c) Pd NPs, d) 2.2Pd-SnO<sub>2</sub> NSs, e) 4.3Pd-SnO<sub>2</sub> NSs and f) 7.5Pd-SnO<sub>2</sub> NSs. g) Volume ratio between H<sub>2</sub> and CO vs. the applied potential on 4.3 Pd-SnO<sub>2</sub> NSs. h) CO and i) H<sub>2</sub> partial current density on SnO<sub>2</sub> NSs, Pd-SnO<sub>2</sub> NSs and Pd NPs. The products at the applied potential (−0.5 to −1.1 V) are collected and quantified by <sup>1</sup>H NMR and gas chromatography (GC).

(2.7–0.54), 7.5Pd-SnO<sub>2</sub> NSs (3.5–0.51) and Pd NP. Notably, the HCOOH production on 4.3Pd-SnO<sub>2</sub> catalyst and 7.5Pd-SnO<sub>2</sub> NSs catalyst is completely inhibited. As illustrated in Fig. 3h and i, Pd-SnO<sub>2</sub> NSs possess higher  $j_{CO}$  and  $j_{H_2}$  than that of SnO<sub>2</sub> NSs, indicating the high activity of eCO<sub>2</sub>RR and HER after the formation of Pd-SnO<sub>2</sub> interface. Though 7.5Pd-SnO<sub>2</sub> NSs catalyst displays the highest  $j_{CO}$  at high current density range, 4.3Pd-SnO<sub>2</sub> catalyst shows larger range of CO/H<sub>2</sub> ratio at the applied potentials, which is apt to control the H<sub>2</sub>/CO ratio. The HCOOH partial current density show that the eCO<sub>2</sub>RR to HCOOH pathway is suppressed on Pd-SnO<sub>2</sub> NSs (Fig. S8).

To gain insight into the kinetics of eCO<sub>2</sub>RR on the Pd-SnO<sub>2</sub> interface, Tafel analysis and electrochemical impedance spectroscopy (EIS) were investigated. As presented in Fig. 4a, 4.3Pd-SnO<sub>2</sub> NSs exhibit the lowest Tafel slope (128 mV dec<sup>−1</sup>) compared with those of SnO<sub>2</sub> NSs (165 mV dec<sup>−1</sup>), 2.2Pd-SnO<sub>2</sub> (143 mV dec<sup>−1</sup>) and 7.5Pd-SnO<sub>2</sub> NSs (136 mV dec<sup>−1</sup>). Fig. 4b shows that Pd-SnO<sub>2</sub> NSs possess the smaller radius than SnO<sub>2</sub> NSs, suggesting the lower charge transfer resistance, which is contributed to the immobilization of Pd on the surface of SnO<sub>2</sub> NSs. These results confirm that the formation of Pd-SnO<sub>2</sub> interface can improve the activity of eCO<sub>2</sub>RR to CO. In addition, the stability of 4.3Pd-SnO<sub>2</sub> NSs was measured at a long-time electrolysis under potential of

−0.6 or −0.9 V. Clearly, both  $FE_{CO}$  and  $FE_{H_2}$  kept constant for 30 h (Fig. 4c). The morphology and valance of 4.3Pd-SnO<sub>2</sub> NSs after electrolysis was characterized by TEM, XRD and XPS. As shown in Fig. S9, no obvious changes in the structures of 4.3Pd-SnO<sub>2</sub> NSs after electrolysis, suggesting that the catalyst is of high stability. In addition, eCO<sub>2</sub>RR performance of 4.3Pd-SnO<sub>2</sub> NSs are evaluated using the flow cell. As shown in Fig. S10, the eCO<sub>2</sub>RR to HCOOH pathway of 4.3Pd-SnO<sub>2</sub> NSs is still suppressed at high current density (>100 mA cm<sup>−2</sup>). The optimal 4.3Pd-SnO<sub>2</sub> NSs exhibit controllable H<sub>2</sub>/CO ratios ranged from 9.2 to 0.26.

### 3.3. Experimental and theoretical study of the catalytic mechanism of Pd-SnO<sub>2</sub> Interface

To clarify the reaction pathways of the catalysts, in-situ ATR-FTIR spectra of the catalyst at different applied potentials were carried out. The peaks at 1542 and 1646 cm<sup>−1</sup> assigned to the characteristic peaks of \*CO<sub>2</sub><sup>−</sup> intermediates, are increasingly apparent on SnO<sub>2</sub> NSs and 4.3Pd-SnO<sub>2</sub> NSs surface (Fig. 4d & e) than that on Pd NPs surface (Fig. 4f), indicating a higher eCO<sub>2</sub>RR activity of SnO<sub>2</sub> NSs and 4.3Pd-SnO<sub>2</sub> NSs than that of Pd [47,48]. When the applied potential was below −0.5 V,

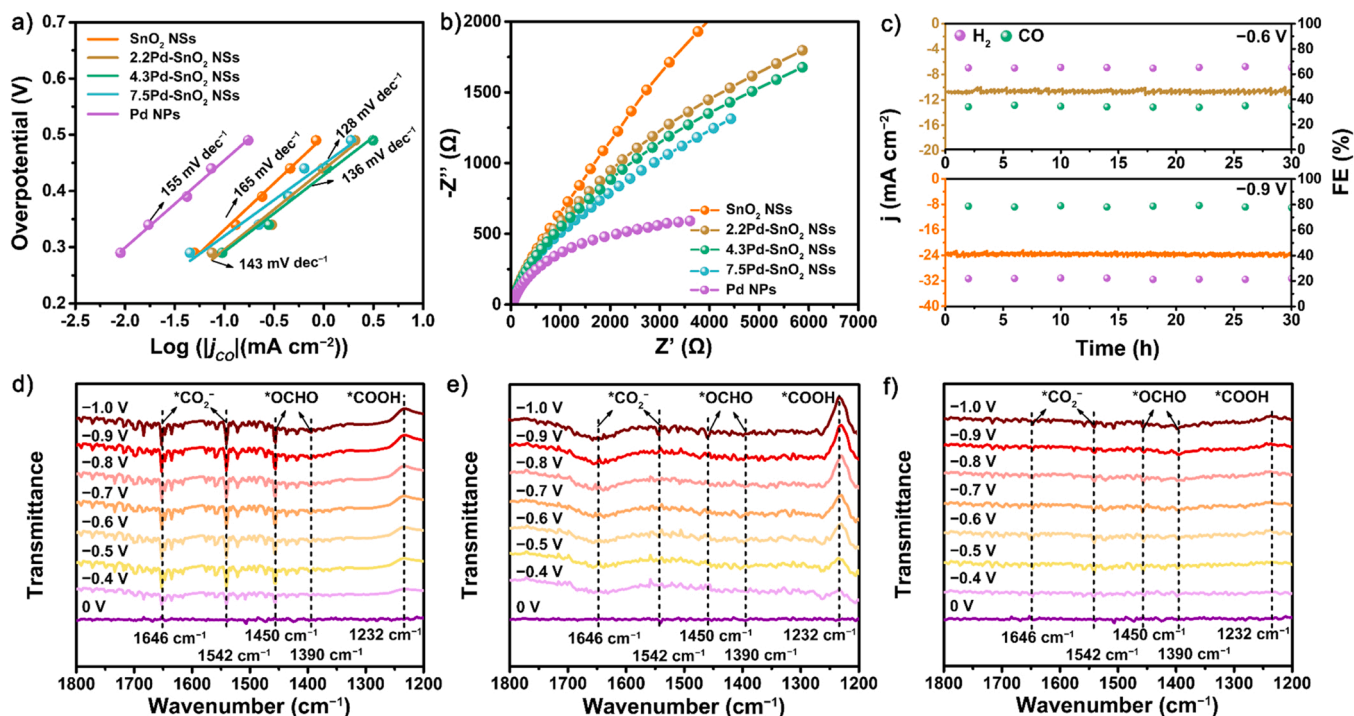


Fig. 4. a) Tafel analysis and b) electrochemical impedance spectroscopy (EIS) of  $\text{SnO}_2$  NSs, Pd-SnO<sub>2</sub> NSs and Pd NPs. c) the stability test for 4.3Pd-SnO<sub>2</sub> NSs at  $-0.6$  and  $-0.9$  eV. In situ ATR-FTIR spectra of d)  $\text{SnO}_2$  NSs, e) 4.3Pd-SnO<sub>2</sub> NSs and f) Pd NPs.

the strengthened vibrational band of  $^*\text{COOH}$  species at  $1232\text{ cm}^{-1}$  appears clearly on 4.3Pd-SnO<sub>2</sub> NSs, but no distinguish peaks can be observed on the surface of  $\text{SnO}_2$  NSs or Pd NPs, which demonstrates that the interface of Pd-SnO<sub>2</sub> possesses high ability to stabilization of the key  $^*\text{COOH}$  intermediates, subsequently promoting the CO pathway. Furthermore, the peaks centered about  $1390$  and  $1450\text{ cm}^{-1}$  assigned to

$^*\text{OCHO}$  species is the key intermediate for HCOOH formation [49,50]. These peaks are not observed on 4.3Pd-SnO<sub>2</sub> NSs and Pd NPs catalysts, confirming that the cooperation of Pd with  $\text{SnO}_2$  can effectively inhibit the generation of HCOOH. Meanwhile, three catalysts show no typical peaks  $^*\text{CO}$  located at  $1900 - 2100\text{ cm}^{-1}$ , suggesting no  $\text{C}_2+$  products pathways (Fig. S11). Consequently, the active Pd-SnO<sub>2</sub> interface can

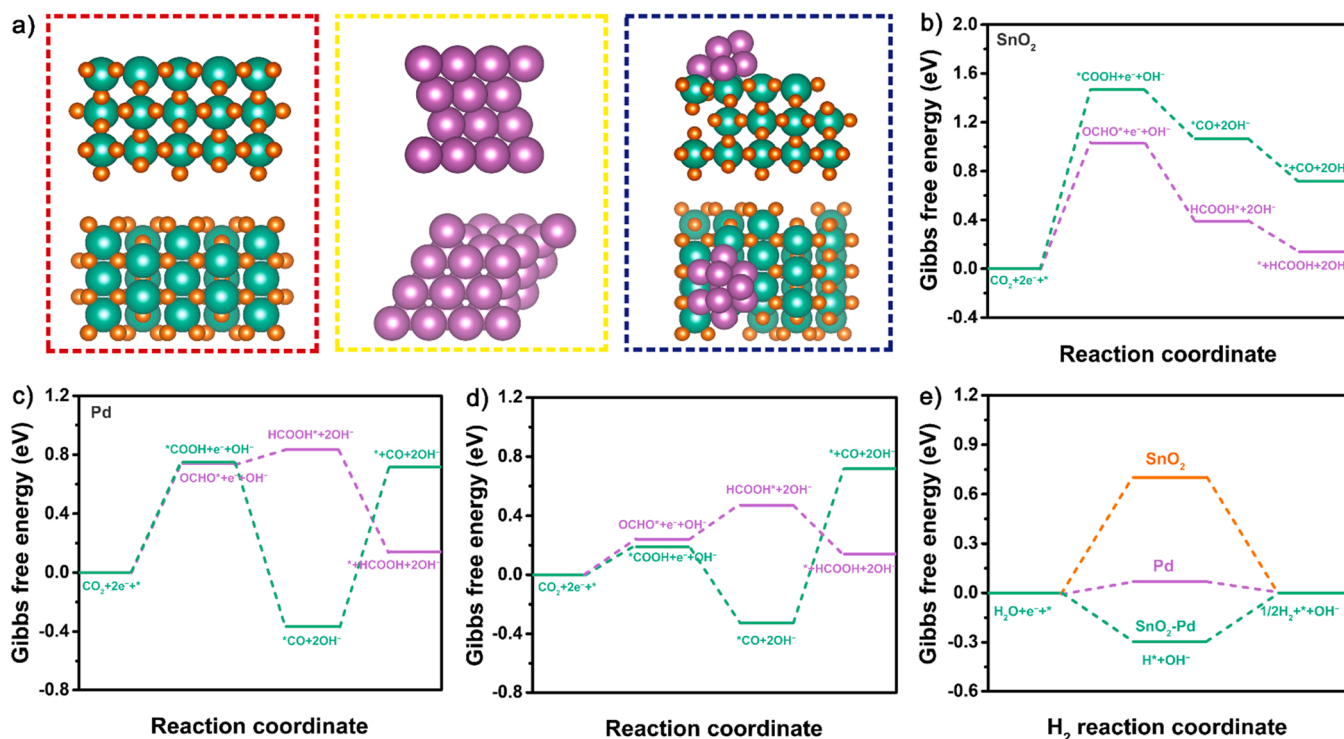


Fig. 5. a) Calculated crystal structure of  $\text{SnO}_2$  (red dotted box), Pd (yellow dotted box), and  $\text{SnO}_2$ -Pd (blue dotted box). The Gibbs free energies of HCOOH and CO reaction coordinate for b)  $\text{SnO}_2$ , c) Pd and d) Pd-SnO<sub>2</sub>. e) The Gibbs free energies  $\text{H}_2$  reaction coordinate.



accelerate the intermediates formation of  $^*\text{COOH}$ , while suppress  $^*\text{OCHO}$  species, thus enhancing the efficiency of syngas production.

To gain insight into the effects of Pd-SnO<sub>2</sub> interface on the thermochemical reaction energy and the adsorption behavior of the key intermediates, density-functional theory (DFT) analysis was performed in the surface-load-type Pd-SnO<sub>2</sub> interface. The models are shown in Fig. 5a. The optimized structures of the reactants and intermediates ( $^*\text{COOH}$ ,  $^*\text{CO}$ ,  $^*\text{OCHO}$ ,  $\text{HCOOH}^*$  and  $\text{H}^*$ ) on SnO<sub>2</sub>, Pd and Pd-SnO<sub>2</sub> models are shown in Figs. S12–S14, respectively. For the eCO<sub>2</sub>RR to CO pathway, Pd-SnO<sub>2</sub> catalyst reveals the energy-favourable trend compared to SnO<sub>2</sub> and Pd (Fig. S15). Specifically, the  $\Delta$  for the formation of  $^*\text{COOH}$  (the key intermediate for CO) on Pd-SnO<sub>2</sub> is 0.19 eV, which is lower than that on SnO<sub>2</sub> (1.47 eV) and Pd (0.75 eV) suggesting that Pd-SnO<sub>2</sub> interface can facilitate CO production. For HCOOH production, the  $\Delta$  for the formation of  $^*\text{OCHO}$  reduce to 0.24 eV from SnO<sub>2</sub> (1.03 eV) and Pd (0.75 eV). However, the  $\Delta$  of  $^*\text{HCOOH}$  on Pd-SnO<sub>2</sub> (0.48 eV) is higher than that on SnO<sub>2</sub> (0.38 eV). Therefore, the dominant reaction pathway varies on three models. On the SnO<sub>2</sub> surface, the  $\Delta$  for the formation of  $^*\text{OCHO}$  and  $\text{HCOOH}^*$  are lower than  $^*\text{COOH}$  and  $^*\text{CO}$  (Fig. 5b), resulting in the ascendant HCOOH production. In converse, on Pd and Pd-SnO<sub>2</sub> surface, the CO pathway is more preponderant on Pd and Pd-SnO<sub>2</sub> as shown in Fig. 5c & d. For the HER pathway (Fig. 5e), the  $\Delta$  for the formation of  $\text{H}^*$  on Pd-SnO<sub>2</sub> (−0.30 eV) is more favourable than SnO<sub>2</sub> (0.70 eV). Consequently, the HER reaction is facilitated on Pd-SnO<sub>2</sub> interface. Therefore, the theoretical results suggest that the Pd-SnO<sub>2</sub> interface could regulate the adsorption and desorption behavior of intermediates, and boost syngas production.

#### 4. Conclusion

In summary, we establish Pd-SnO<sub>2</sub> catalysts for eCO<sub>2</sub>RR to syngas. The catalysts show great potential to control the eCO<sub>2</sub>RR and HRE processes, suppressing the HCOOH selectivity for efficient syngas production with controllable H<sub>2</sub>/CO ratios. The optimal 4.3Pd-SnO<sub>2</sub> catalyst exhibit a competitive activity for CO and H<sub>2</sub> generation. The H<sub>2</sub>/CO ratio can range from 4.2 to 0.28 by adjusting the applied potential. Moreover, the H<sub>2</sub>/CO ratio can effectively maintain under a long-term durability test of 30 h. Electrochemical test and theory calculations demonstrate that with the formation and increasing of Pd-SnO<sub>2</sub> interface, the active Pd-SnO<sub>2</sub> interface accelerates the intermediates formation of  $^*\text{COOH}$ , and suppresses HCOOH pathway, thus improving the selectivity of CO for controllable H<sub>2</sub>/CO ratios of syngas production. This work unfolds a promising candidate for earth-abundant Sn-based electrocatalysts towards CO<sub>2</sub> electroreduction to syngas.

#### CRediT authorship contribution statement

**Haichuan He:** Conceptualization, Methodology, Investigation, Formal analysis, Visualization, Writing – original draft, Reviewing and editing. **Dan Xia:** Conceptualization, Validation, Formal analysis. **Xiao Yu:** Investigation, Visualization. **Jian Wu:** Data curation. **Yan Wang:** Data curation, Formal analysis. **Fei Chen:** Data curation, Investigation. **Dr. Liqiang Wang:** Data curation. **Dr. Linlin Wu:** Conceptualization. **Dr. Jianhan Huang:** Conceptualization, Methodology, Visualization. **Dr. Ning Zhao:** Methodology, Visualization. **Dr. Liu Deng:** Conceptualization, Methodology, Visualization, Writing – original draft, Writing – review & editing. **Dr. You-Nian Liu:** Corresponding author, Supervision, Conceptualization, Writing – original draft preparation, Reviewing and editing.

#### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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#### Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.apcatb.2022.121392.

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